

- the volume of mesopores with a diameter of between 40-150 Å, and a mean diameter of between 80-120 Å represents 30-80% of the total pore volume,
- the volume of macropores with a diameter that is greater than 500 Å represents 20-80% of the total pore volume, and
- a specific surface area that is greater than 200 m²/g.

2. (Amended) A catalyst according to claim 1, in which the silica-alumina comprises Al_{VI} (octahedral) radicals and Al_{IV} (tetrahedral) radicals, whereby the proportion of the tetrahedral Al_{IV} is between 20 and 40%.

3. (Amended) A catalyst according to claim 1, in which the silica-alumina comprises 30-50% of Q² radicals, in which an Si atom is linked to two Si or Al atoms and to two OH groups and also comprises 10-30% of Q³ radicals in which an Si atom is linked to three Si or Al atoms and to an OH group.

4. (Amended) ~~Catalyst~~ A catalyst according to ~~one of the preceding claims~~ claim 1, that contains boron and/or silicon.

5. (Amended) A catalyst according to claim 1, that contains at least one element that is selected from among groups VIIA, VIIB, and VB.

6. (Amended) A catalyst according to claim 1, in which the substrate is constituted by silica-alumina.

7. (Amended) A catalyst according to claim 1, whose substrate comprises 1-40% by weight of binder.

8. (Amended) A catalyst according to claim 7, in which the substrate results from the mixture of said silica-alumina and at least one binder that is selected from the group that is formed by silica, alumina, clays, titanium oxide, boron oxide and zirconium.

9. (Amended) A catalyst according to claim 1, that has undergone a sulfurization treatment.

10. (Amended) A process for hydrocracking with a catalyst according to claim 1, at a temperature that is greater than 200°C, a pressure that is greater than 0.1 Mpa, with an amount of hydrogen of at least 50 l/l of feedstock, and with an hourly volumetric flow rate of 0.1 to 20 volumes of feedstock per volume of catalyst and per hour.

11. (Amended) A process according to claim 10 for the hydrocracking of feedstocks that are selected from the group that is formed by kerosenes, gas oils, vacuum gas oils, atmospheric residues, vacuum residues, atmospheric distillates, vacuum distillates, heavy fuels, oils, waxes, paraffins, waste oils, deasphalted residues, deasphalted crudes, the feedstocks that are obtained from thermal conversion or catalytic conversion processes, whereby the feedstocks contain less than 30% by weight of paraffins.

12. (Amended) A process according to claim 10, wherein the feedstock is first hydrotreated.

13. (Amended) A process according to claim 10, in which the hydrocracking is carried out in two stages with intermediate separation, whereby the catalyst is used in at least one stage.

14. (Amended) A process according to claim 10, in which the feedstock contains less than 25% by weight of paraffin.

Please add the following new claim:

- 15. A catalyst according to claim 1, wherein the volume of macropores in said silica-alumina is 20-70% of the total pore volume.--

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